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# WP7 Biokinetic Data, Modelling and Control

2<sup>nd</sup> year CROPGEN meeting, 6<sup>th</sup> February 2006, Vienna

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# Objectives



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- Further development of an existing Anaerobic Digestion Model
- Implementation of this model in a web-based Virtual Laboratory (VL)
- Basis of the VL is the Anaerobic Digestion Model No.1 (Batstone *et al.*, 2002)
- Creation of a Decision Support System
- Identification of process-control strategies and fermentation mixtures

# Anaerobic Digestion Models



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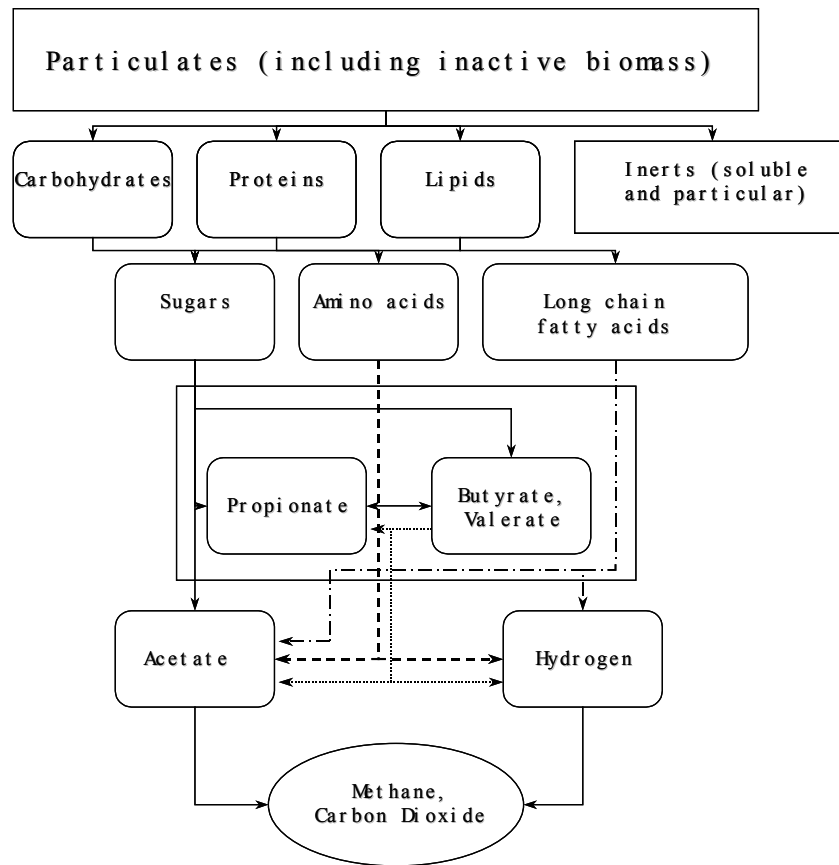


- Hydrolysis controlled Anaerobic Digestion (Jain *et al.*, 1991)
- Model for Dynamic Simulation of Complex Substrates - Focusing on Ammonia inhibition (Angelidaki *et al.*, 1993)
- Simulation Model <Methane> (Vavilin *et al.*, 1993)
- Comprehensive Model of Anaerobic Bioconversion of Complex substrates (Angelidaki *et al.*, 1998)
- Model for Meso- and Thermophilic Anaerobic Sewage Sludge (Siegrist *et al.*, 2002)
- Anaerobic Digestion Model No.1 (ADM1) (Batstone *et al.*, 2002)

# Anaerobic Digestion model No.1 (ADM1)



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- Model is structured in several steps characterising the biochemical processes
- DAE: 26 dynamic state variables  
19 biochemical kinetic processes  
3 gas-liquid transfer kinetic processes
- DE: 32 dynamic state variables  
6 acid base kinetic processes
- Implementation in a CSTR

# Anaerobic Digestion model No.1



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## Advantages



- First unified model
- Unified Nomenclature and Kinetics
- Basis for further model approaches
- Describes Process Details
- Lower overall data amount compared to Neuronal Networks

# Anaerobic Digestion model No.1



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## Disadvantages

- Need to understand the model
- The model is simplifying the AD process
- No validation of biological parameters
- No information on the effect of inhibitory compounds
- No information on the effect on kinetics in different temperature ranges
- Requirement of detailed substrate definition
- The COD flow is rather complex

# Anaerobic Digestion model No.1



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- Solid Precipitation
- Homoacetogenesis
- Acetate Oxidation
- Lang Chain Fatty Acids Inhibition
- Weak Acid and Fatty Acid Inhibition
- Denitrification
- Sulphate Reduction and Sulphide Inhibition
- Glucose Fermentation



# Anaerobic Digestion model No.1



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## Parameter

	Min	Max	
$k_{dis}$	0,25	1	$[d^{-1}]$
$k_{hyd,ch}$	0,041	106	$[d^{-1}]$
$k_{hyd,pr}$	0,0096	10	$[d^{-1}]$
$k_{hyd,li}$	0,0096	10	$[d^{-1}]$
$k_{m,su}$	4	5067	$[kg_{cod}kg_{cod}^{-1}d^{-1}]$
$k_{m,aa}$	0,5033	53	$[kg_{cod}kg_{cod}^{-1}d^{-1}]$
$k_{m,fa}$	0,6	363	$[kg_{cod}kg_{cod}^{-1}d^{-1}]$

- Parameters quoted in the ADM1 have a high range of margin
- Parameters suggested from the Task group are suitable for sewage sludge
- Not suitable for energy crops

# Anaerobic Digestion model No.1



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## Implementations, Extensions and Adaptations of the model



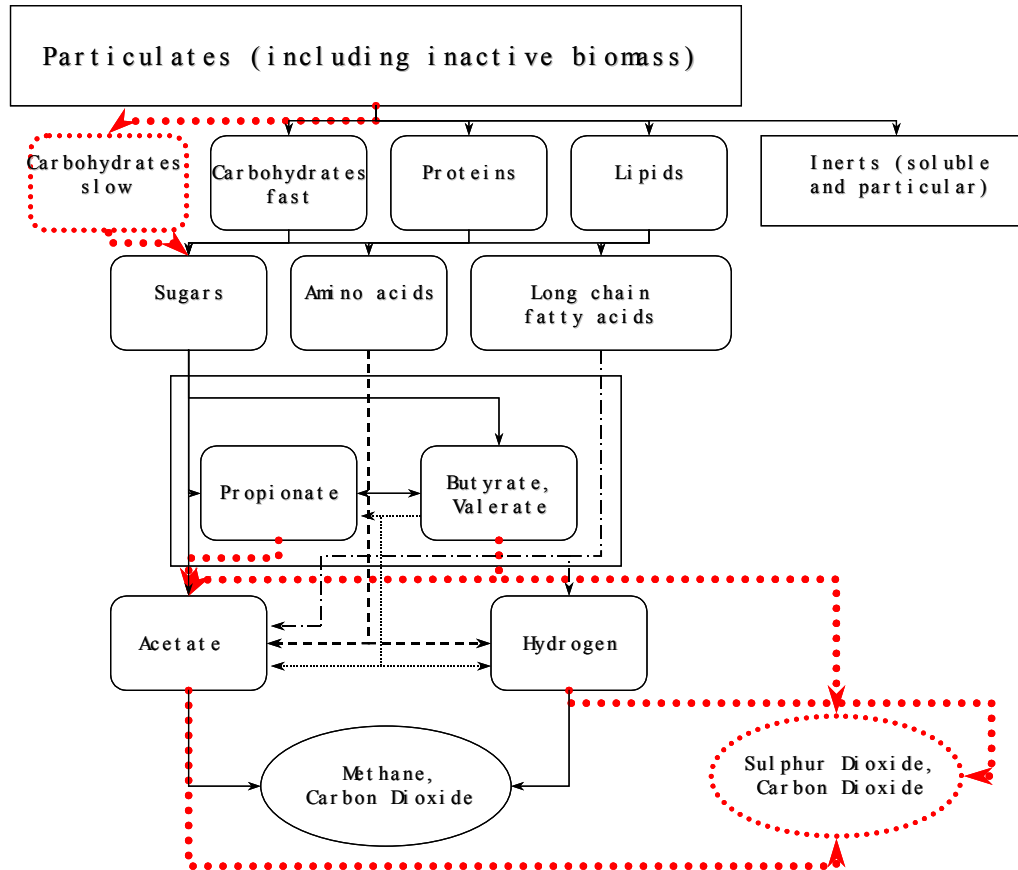
- $\text{CaCO}_3$  precipitation and the potential of anaerobic digestion in the thermophilic temperature range (Batstone et al., 2003)
- Modelling of two-stage anaerobic digestion using the IWA Anaerobic Digestion Model No. 1 (ADM1) (Blumenstaat and Keller, 2004)
- ADM1 based virtual plant for the validation of a controller [TELEMAC] (Mailleret et al, 2004)
- Benchmark study Modelling Sulphate Reduction using NN and ADM1 (Strik *et al.*, 2004)
- Application of the Adm1 model to advanced anaerobic digestion (Parker, 2005)

First International Workshop on the IWA Anaerobic Digestion Model No.1 (ADM1),  
2<sup>nd</sup> – 4<sup>th</sup> September 2005 in Lyngby, Denmark

# Adaptation of the ADM1



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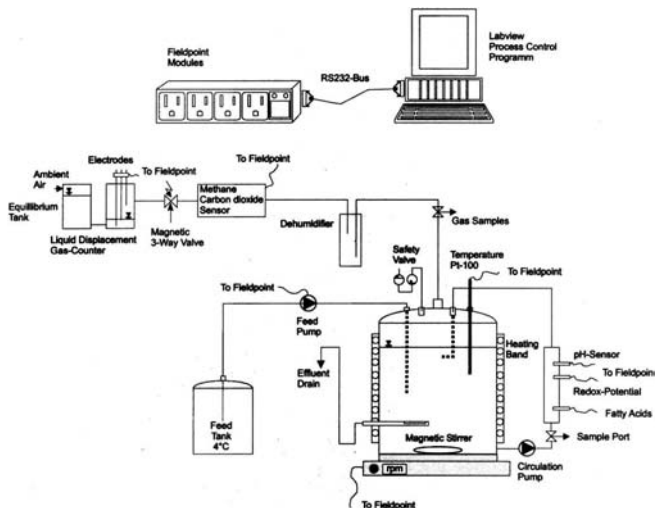


# Laboratory Experiments

## Lab-scale anaerobic CSTRs



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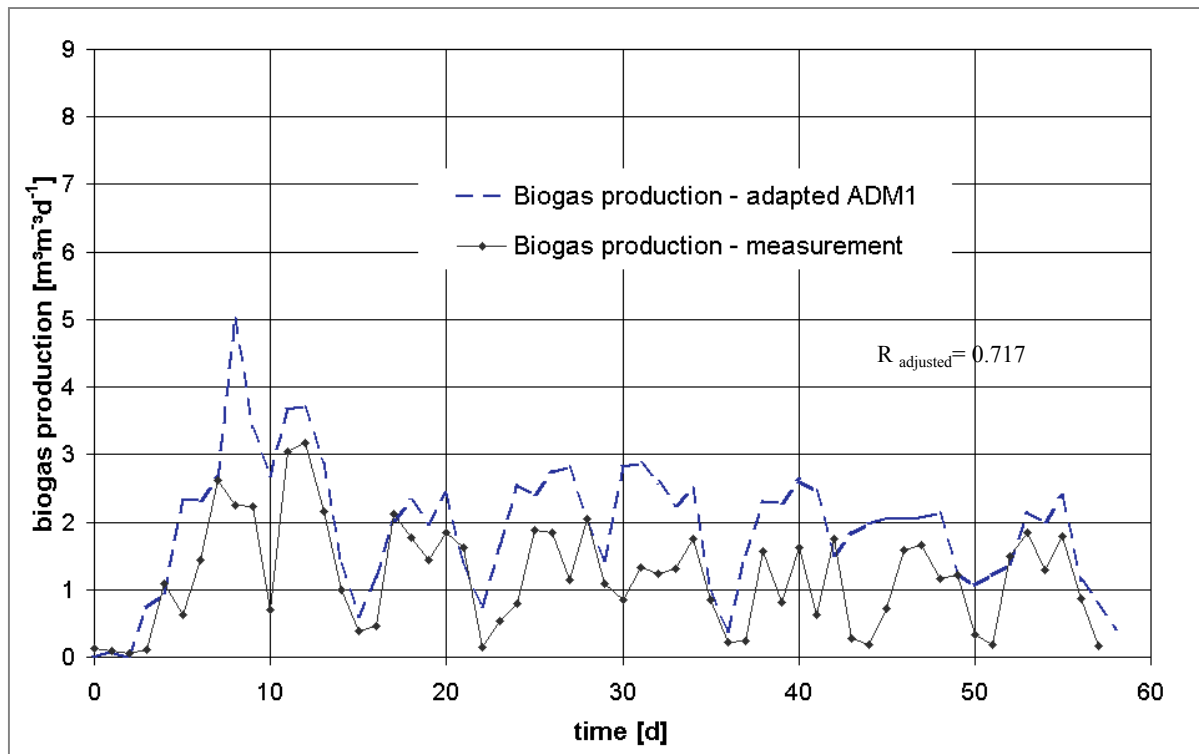


# Anaerobic Digestion model No.1



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## Model Results

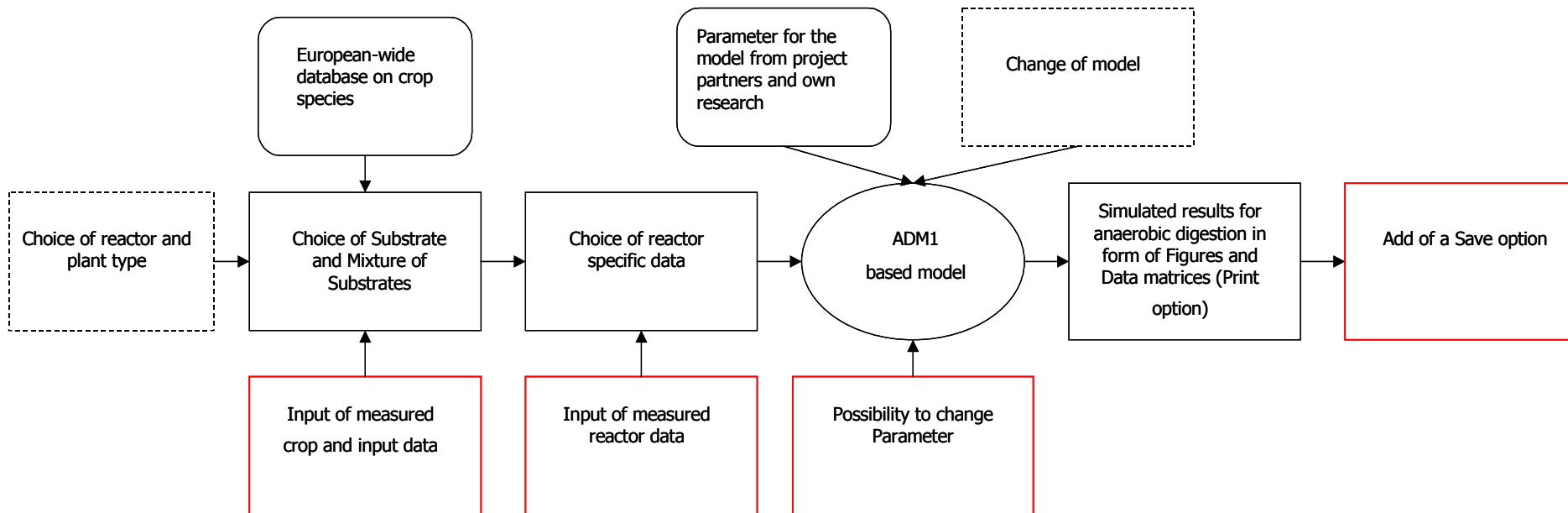


# Virtual Laboratory



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## Structure



# Virtual Laboratory



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## Screenshot 1

The screenshot displays the CROPGEN virtual laboratory interface. On the left, there are four choice boxes (Choice 1 to Choice 4) with dropdown menus and corresponding percentage input fields. Choice 1 is set to 'Mais' and 100%. Choices 2, 3, and 4 are set to 'no input' and 0%. A 'Sum percentage' field shows 0%. A large 'STOP' button is located below these fields. In the center, a text box instructs the user to input feed amount (mass, volume, or organic loading rate) and to push the 'Feed' button. Below this is a 'Feed' input field set to 0 and a unit dropdown set to 'kg/d'. On the right, a temperature selection field is set to 0 °C, with a note to choose between 30 °C and 60 °C. Below it, a pressure field is set to 1,0325 bar. At the bottom, there are two volume fields: 'Volume reactor - liquid phase' and 'Volume reactor - gas phase', both set to 0 m³. At the bottom right, there are two buttons: 'OK' and 'STOP'.

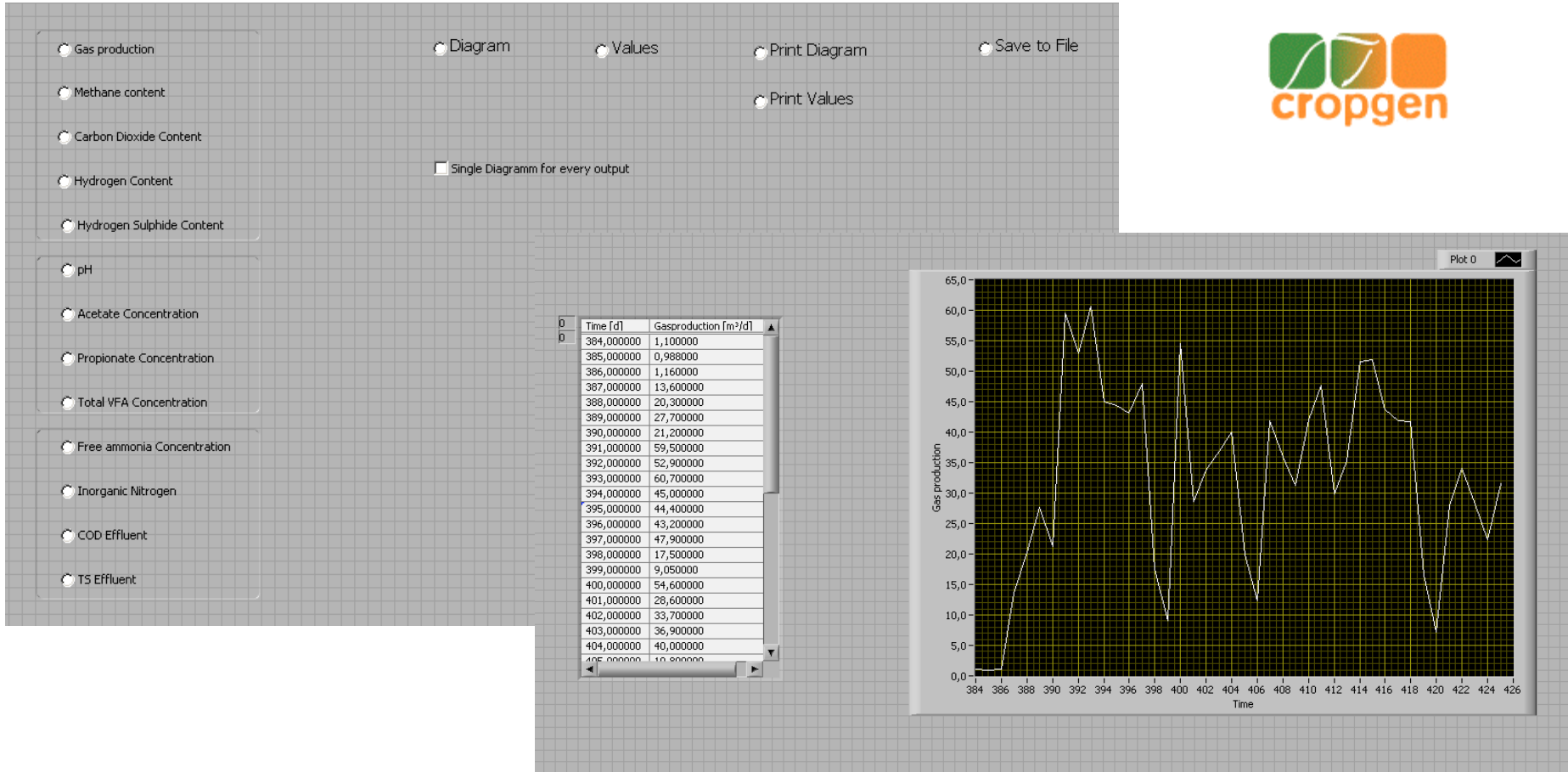


# Virtual Laboratory



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## Screenshot 2





# Summary & Conclusion



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- Since 60s large amount of different AD models
- ADM1 as first unified model
- Adaptation of the model
- Required parameters and measurement
- Adapted ADM1 as basis for a Virtual Laboratory
- 2 Versions of the VL (Simple and Advanced)
- Mathematical model as basis for a control tool



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**Thank you for your attention.**



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